

DEPARTMENT OF MECHANICAL ENGINEERING

LECTURE NOTES

ON

FLUID MECHANICS

4th SEMESTER, MECHANICAL

By

Er. Santosh Nayak
Lecture in Mechanical Engineering
B.IE.T, MOHADA (BAM)

506: - FM (Fluid Mechanis) SET-1 Full Maruey - 80

Time-3 hours.

Answer cury fine questions including question NO-01, and 02.

- (1) (a) Define specific weight and specific granity. (2×10)
 - (c) Define the torm viscocity
 - (d) Write Anchimedis's preinciple.
 - (e) Define metacentre and metacentraic height.
- (f) what is the difference between laminar and turbulent flow?
- (9) what is pitol tube?
- (h) state Dancy's formely for loss of head in pipe?
- (is what do you mean by impact of jet !
- (j) What is venacontracta?
- (2) Answer any fine.

5 X 6

- (i) with near sketch emplain the working of Bourden's tube pressure gauge.
- () Derive an equation for the total pressure on a verdical immerged surface.
- (iii) The diameter of a pipe at the section 1 and 2 are 10cm and 15cm respectively. Find the discharge through the pipe if the velocity of water flowing through the pipe at section B is sm/s. Find the velocity at section 2.
- (iv) write down the expression of loss of energy due to friction amoraling to Davay's formula and chery's formula with proper notation.

- (V) A sharp-edges orifice of 5 cm diameter discharges water under a head of 45 m. Determine the coefficient of discharge is the measures rate of flow is 0.0122 m²/₂.
- (vi) Derive an expression for the force of jet on a. finest plate.
- (3) A rectangular plane surface is 2m wide and 3m deep. It lies in writical plane in water. Determine the fotal pressure and position of centre of pressure on the plane surface when its upper edge is heritantal and councides with the water surfaces. The total pressure and position of centre of pressure when the upper edge is 2.5m below the free water surface.
- (4) Describe the orifice coefficients and write down 10 the relationship among them.
- (5) Water flows through a pipe of 200mm in elicuration and Gom long with a velocity of 2.5 m/s. Find the head lost due to fraction using

 (a)Dancey's formula , f=0.005

 (b) Chery's formula C=55.
- (6) Derive Bernoulli's equation and state the prientical application in venturimeter.
- (7) A jet of water 40 mm cliamler moving with a velouity of 120 m/s impinging on a review of varies [10] moving with a velocity of 5 m/s ec. Finel the force eneroled, workdone and efficiency.

All The Best.

Full Manist - 20

Time - 3 hours

Anuen cuny fine questions including question No. 01 and 02.

Dar Define density and state its unit.

12×10

(ii) Derkne pascul's law.

(iii) Define the team sunface tension.

(N) What is the function of pierometer ?

(v) Define Bouyanny force ?

(vi) what is the difference between compressible and incompressible their?

(vii) what are the assumptions taken in deriving the Bernoulli's equation.

(viii) what is chery's constant?

(1x) Define hydraulic greationet?

(n) Define pressure head and relocity head.

(2)(1) Explain absolute pressure, celmosphereic pressure and gauge
pressure and state their relations.

(ii) Explain the working and function of a pitot tube.

(iii) A simple U-tube manameter containing mencury is connected to a pipe in which fluid of specific grancity o.8 and having vaccum pressure is flowing. The other end of the manometer is open to atmosphere. Find the vacuum pressure in the pipe if the difference of vacuum pressure in the pipe if the difference of mencuy level in the two limbs is your and the nearly level in the left from the centre of height of fluid in the left from the centre of pipe is 15 cm. below.

(iv) Derive workingity equation.

- (V) water 11 flowing through a pipe 1500 m long and 400 mm diameter with a relocity of 0.7 m/s. What should be the diameter of pipe if the loss of head die to friction in 8.7 m. Take of for the pipe in 0.01.
- (vi) Enplain hydraulic gradient and total gradient line.
- (3) Describe different types of manometers.
- (4) The head of water over an orifice of diameter yours in 10m. Find the actual discharge and actual velocity of jet at vena contracta. take (d = 0.6, Cv = 0.98.
- (i) The discharge over a rectangular notch is 0.135 m3/s when the wellers level is 22.5 m echove the still. if the welficent of discharge is 0.6 find the 15 leneth of notch.
- (5) Derive an enprovion for the force of jet on a [10] fined and inclined picel-e.
- (6) Describe different types of flows.
- (7) Derive the expression of actual discharge in 10 venturimeter and state its practical applications.

All The Best.

Introduction .

A notch is a clevice used for measuring the reste of flow of a liquid through a small channel or a tank.

If may be defined as an opening in the ricle of a tank on a small channel in such a way that the liquid surfaces in the tank or channel is below the top edge of the opening.

pen chainer over which the flow occurs. It is generally in the form of ventical wall with a sharp edge cet the top.

The notch is of small size while the weir is of a bigger sère.

The notch is generally made of metallic plate while the wein is made of concrete structure.

clamitication

The notches are claufied as

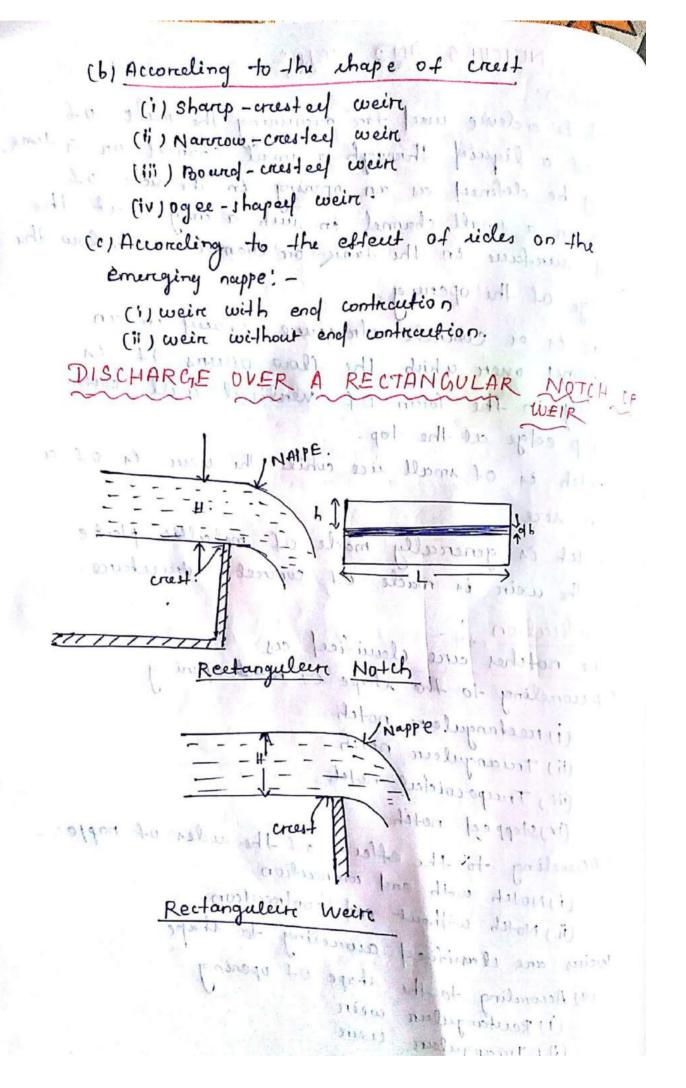
- O According to the shape of motels opening
 - (i) reetangular notch
 - (11) Treianguleur notch
 - (iii) Traporoidal notch

(iv) stepped notch.

- (i) Notch with end contraction
 - (ii) Notch without end confraction.

weires are clamified awreling to shape

- (9) According to the shape of opening
 - (1) Reutanguler wein
 - (ii) Triangulaire weire
 - (iii) Trapezoidal wein.



comider a rectanguleur notch or weir provided in a channel centraging water.

H = head of water over the crest L = Length of the notch or weire.

To find the direhange of water flowing over the weir on notch, consider an elementary horizontal strip of water of thickness of and horizontal strip of water of thickness of warface. length L at a depth h from the free wintage.

Arees of strip = Lxdh.

theoretical velocity of water Alowing through strip = 129th

The discharge do, through straip is

des = Cox area of strip x Theoretical relocity

$$Cl = \int Ccd \times L \times \sqrt{2gh} \times dh$$

$$= Ccd \times L \times \sqrt{2g} \times \int h^{1/2} dh$$

$$= cd \times L \times \sqrt{2g} \times \int h^{1/2} + 1 \int_{0}^{1/2} dh$$

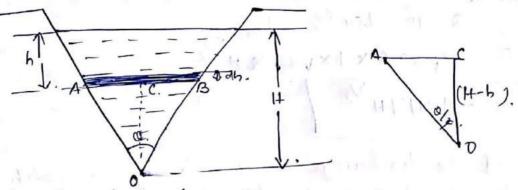
$$= de cd \times L \times \sqrt{2g} \times \int h^{1/2} + 1 \int_{0}^{1/2} dh$$

$$= \operatorname{ecd} \times \operatorname{L} \times \sqrt{29} \times \frac{h^{3/2}}{3/2} \int_{0}^{4}$$

$$g = \frac{2}{3} c_4 L \sqrt{29} \times (H)^{3/2}$$

Expired the discharge of water flowing over rectangular notch of 2m length when the comband hery over the notich it 300 mm. Cof =0.60 Head over the notch! H = 300 mm = 0.30m Ca = 0.60 mm de L = 2 m Q = 2/3 Cdx Lx \(\frac{29}{29}\times (H^3/2) $= \frac{2}{3} \times 0.6 \times 2.0 \times \sqrt{2 \times 9.81} \times (0.30)^{3/2}$ CS = 0.582m3/s: 0x1-quil 2000 a) Defermine the height of a prentangular every length 6m to thebe built oursons, a restangular channel. The manimum length of water on the upstream vide of the wir is 18 m and discharge 2000 litro /s. take ('Cd = 0.6) L=6m. H1=1.8 m Q = 2000 lt/s. 1 x dg c Hr 1+3 Q = 2/3 Cd X L XV 29 x H 3/2 => 2 = 3/3 0 x 0. 6 x 6. 0 x \(\sqrt{2x 9.81} \) x H 3/2 = H^{3/2} = $\frac{2.0}{10.623}$ H = 0.928m = 1.8-0.328 = 1.472m

TRIANGULAR NOTCH OR WEIR DISCHARGE



H=head of western cubone the V-notch

a = angle of notch.

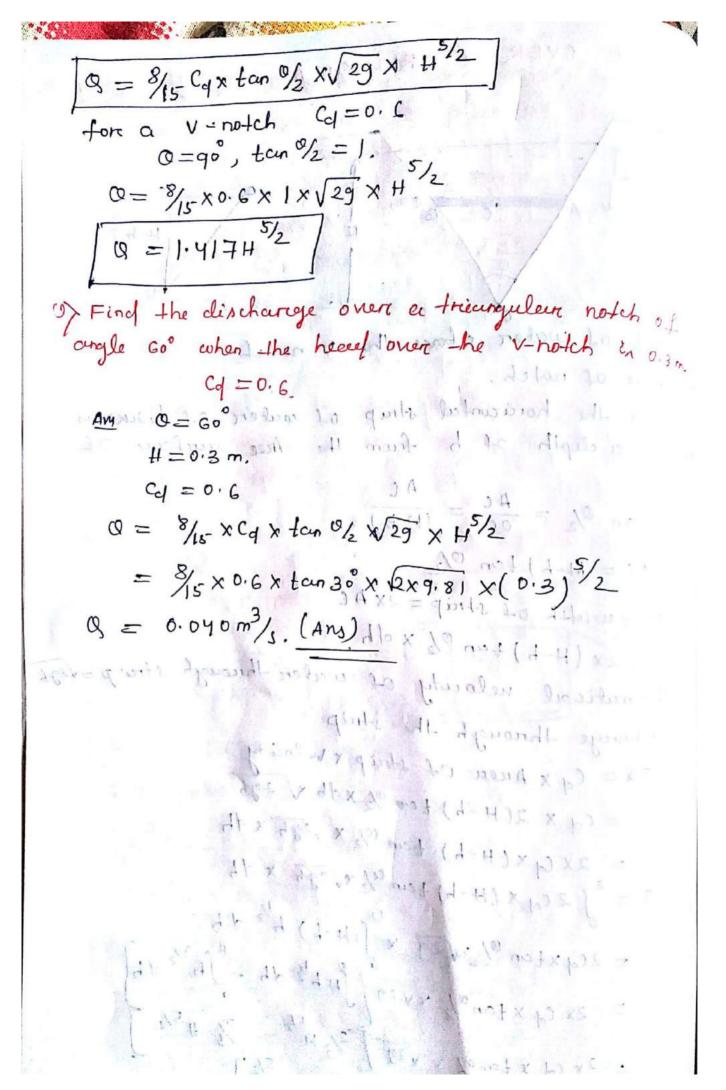
comider the horizontal strip of water of thickness 'dh' at a clepth of h from the free unifour of water.

$$\tan \frac{Q}{2} = \frac{AC}{OC} = \frac{AC}{(H-h)}$$

AB = width of strip = 2x AC

= 2x (H-h) tan 0/2 x dh

theoretical relacity of water through stree p = 1296 Discharage through the strip



FLOW THROUGH PIPES (CHAPTER-6)

Loss of energy in pipe!

when a fluid in flowing through a pipe, the theird experiences some remistance due to which of the energy of fluid in lost. This loss of energy in clauficel as follows.

Eenergy loss

Major energy loss

In Lach Cur.

Then in due to freition. (a 1 Darcey - Weis beech formules. (b) cherry's Formula.

Minor energy loss

(9) Sudden expansion of pipe (1), suelden contraction of pipe

(c) Bend in pipe.

(d) pipe fellings me, obstruction in pipe.

(1) LOSA of energy due to friction.

(a) Dury-Weisbarch Formula!

This low of energy in pipes due to friction in calculated from Dancy - Weisbach equation. $h_f = \frac{4 + L V^2}{29 + Q}$

hy = LOM of head due to fraction. f = coefficient of friction = 16
Re

$$f = \frac{16}{Re} \left(Re < 2000 \right)$$

$$f = \frac{0.079}{te^{1/4}} \left(Re \left(4000 - 10^{6} \right) \right)$$

$$L = Length of pipe.$$

V= mean relowity of flow

of = diameter of Pipe.

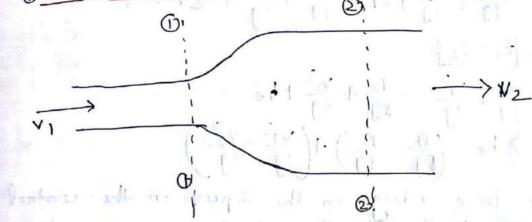
(b) chezys formula The enpression for loss of hered due to frieto. hf = fl x Ax,LXV2 hf = loss of head due to friction A = area of cross-section of Pipe p = wetter perimeter of pipe v = mean nelocity of flow less thank p = percimeters of pipel. L = Length of pipe. A = Arcea of flow is called hydraulic meandy A = (hydraulic meen depth on hydraulic rading) (Ap) in denoted by m'. mobile of mil .. hydraulin mean depth m= 4/p= Try of = (4) A = m on (A) = /m. $h_f = \frac{f}{fg} \times L \times \sqrt{2} \times \frac{1}{m}$ => v = \frac{f!}{f!} x m x (\frac{ht}{L}) \frac{1}{2} \quad $\Lambda = \frac{1}{30} \times \frac{1}{20} \times \frac{1}{$ where \frac{fg}{11} = c (c'=chezy's constant) $\frac{1}{L} = (i - i)$ This Is known as chery's formulas.

```
Q), Find the head lost due to fruition in a
  pipe of diameter 300mm and length 50 m
 through which water it -Bowing at a relouty
 of 3m/s . wing
         (11 Daring's formules Data Y = 0.01 stone)
          (ii) chery's formules.
       d = 300mm = 0.30m.
                          1 = 0.01 2 to ive = 0.01 x 10-4 m3/3
       v = 2m/s.
       C = Go .
       You and
        Re = \frac{Vd}{V} = \frac{3 \times 0.30}{0.01 \times 10^{-4}} = 9 \times 10^{5}
      f = \frac{0.079}{\text{Re}^{1/4}} = \frac{0.079}{(9 \times 10^{5})^{1/4}} = 0.0025^{-6}.
 (i) hf = 4xfx Lxv2 · (Franciska formules)
           = \frac{4x f x L x v}{4x 2g}
= \frac{4x 0.0025 6 x 50 x 3}{0.3 \times 2 \times 9.81}
      hf = 0.7828 m (Ans)
 (ii) chezy's formules.
       C = 60., m = \frac{d}{4} = \frac{0.3}{4} = 0.075 m
  V = c \times \sqrt{mi}
\Rightarrow 3 = 60 \times \sqrt{0.075 \times \frac{h_f}{L}}
  => (=3) = 0.075 × hit
   \Rightarrow \frac{h_{1}}{L} = \left(\frac{3}{60}\right)^{2} \times \frac{1}{0.075}
    => ht = (3) 2 x 0.075 x 50 = 1.665 m. (And)
```

Minor Energy Losses:

The loss of energy due to frietion in pipe is
Known ess major loss while the loss of energy due to
change of relocity of the for fluid is called minore
loss of energy.

OLOMA Of head due to medden enlangement-



consider a liquid flowing through a pipe which has sudden enlargement as shown on ratione tigure.

consider two rections O-O and O-O before and after enlargement.

P₁ = pressure intensity at section 0-0 v₁ = velocity of flow at section 0-0 cu₁ = arcsec of pipe at section 0-0. P₂ = pressure intensity ut section 2-2 v₂ = velocity of flow at section 2-2 v₂ = area of pipe at section 2-2 a₂ = area of pipe at section 2-2

Due to sudden change in diameter of pipe from D1 to D2, the liquid flowing from the smaller pipe is not able to follow the change of boundary. Thus the flow separates from the boundary and turbulent eddies are formued.

A TO THE PARTY OF THE PARTY OF

The loss of energy toures planes oleve to form, of those eddies:

p'= pressure internity of the liquid eddies he = LOM OIL head du to suelden enlangement Applying Bernoulli's equation P1 + V12 + Z1 = P2 + Z2 + L2 + head long \Rightarrow $|z_1 = z_2|$ $\frac{p_1}{39} + \frac{v_1^2}{29} = \frac{p_2}{39} + \frac{v_2^2}{29} + he$ => he = (P) - 12) + (V1 - V2) -> The force acting on the liquid in the control volume in the direction of flow is given by Fx = P. A++P (A2-A1)-P_A2 11 - 1000 sections (1-1-2) (- 1-1-19 0 - 1-Fx = P1 A1 +P1 (A2 -A1) -P2A2 = P1A2 - P2A2 Fx= Az (P1-Pz) inistra inuisang Momentum of liquid in section 1-1 = 8,AIV,2 momentum of liquid at section 2-2 = 9 A2V2 change in momentum = \$A2V2 - 8 A1V, 2 continuity equelion [AIVI = AZVZ] $A_1 = \frac{A_2 V_2}{V_1}$ change in momentum/sec = & A2V22- & x A1V12 $= fA_2V_2^2 - g \times A_2V_2 \times V_2^2$ = 8 Azvz2 = 8 Azvivz = \$ A 2 (V2- V1 V2)

Net force certing on control volume en the direction of flow must be equal to the reale of change of ntum . $(P_1-P_2) \cdot A_{27} = SA_2 (V_2^2 - V_1 V_2)$ $\frac{1}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{\sqrt{2}}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2} - \sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{2}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{\sqrt{2}}{\sqrt{2}} = \frac{2$ 7 1-P2 - V2-V1V2 Described the 100 1-10 100 ... he = $\left(\frac{P_{13}}{89} - \frac{P_{2}}{89}\right) + \left(\frac{v_{1}^{2}}{29} - \frac{v_{2}^{2}}{29}\right)$ $= \frac{v_2^2 - v_1 v_2}{9} = + \frac{v_3^2}{29} = \frac{v_2^2}{29} = \frac{v_3^2}{29} = \frac{v_3^$ 2v2 - 2v1v2 + v12 - v22 of the only of thow all 2-2. he = Ne -10)2 he = $\frac{(v_1 - v_2)^2}{2g}$ Sudden Contraction Low of Head due to Sudden Contraction

> Comider a liquid flowing in a pipe which has sudden contraction in around as about in fig. 4 > comider two section (1-1) and (2-2) before and after contraction.

→ An the liquid goes from a larige pipe to a small pipe, the area of flow goes on decreasing and becomes minimum at section (C-1). This rection of it called as were confracted.

After rection (-1, a medden enlargement takes plans
The low of head due to medden contraution in
actually due to medden enlargement from
vera contracte to maller pipe.

Let Ac = Area of flow at rection C-i.

Vc = relowity of flow at rection C-C.

Az = Area of flow at rection 2-2.

Vz = relowity of flow at rection 2-2.

hc = LOAA of head deed to rudden contraction.

$$h_{c} = \frac{(v_{c} - v_{2})^{2}}{2g}$$

$$= \frac{v_{2}^{2}}{2g} \left[\frac{v_{c}}{v_{2}} - 1 \right]^{2}$$

from continuity equation $A_c V_c = A_2 V_2$ $\frac{V_c}{V_2} = \frac{A_2}{A_c}$ $\Rightarrow \frac{V_c}{V_2} = \frac{1}{c_c}$ $h_c = \frac{V_2^2}{2q} \int \frac{1}{c_c} - 1$

where $K = \left(\frac{1}{C_c} - 1\right)^2$ he = KV121 11 10000 10 may sell 12 may The moving trapely is really princh of and of feeling Cc = 0.62 kp. K = (0.62 -1) = 0.375 hc = 0.3.75 \frac{\v2^2}{2.9} \langle \quad \qq \quad gf the 4 value in not given then $\frac{h_c = 0.5 \frac{v_2^2}{2cq}}{}$ (2) Final - the low of head when the pipe of dianet en 200 mm is meddenlig enlariquel to a diameter of youmm. The rate of flow of water through the pipe on 250 litro/see. $D_1 = 200 \text{ mm} = 0.2 \text{ m}$ $D_2 = 400 \text{ mm} = 0.4 \text{ m}$ $A_1 = \sqrt{1/4} 9_1^2 = \sqrt{1/4} \times (0.2)^2 = 0.03 \text{ M/m}^2$ A = T/4 D2 = T/4 × (0.4)2 = 0.12564 m2 cl = 250litn/s = 0.25 m3/s. VI = 0/AI = 7.96 m/s who had to make - di $V_1 = \sqrt[4]{A_1} = \sqrt[4]{A_2} = \sqrt[4]{99} / \sqrt[4]{99} = \sqrt[4]{99} = \sqrt[4]{99} / \sqrt[4]{99} = \sqrt$ = 1.816 m of water. (Ans) 1 2 vx

3) Loss of Head at the fortrance of Dipe. This is the loss of energy which occurry when a liquid enteres a pipe cohich is connected to large tank. $hi = 0.5 \frac{\sqrt{2}}{29}$ v = relowity of liquid in pipe. 4) LOM of Head at the Enit of pipe ! -This is loss of head due to relocity of liquid at the outlet of pipe: 9+ in elenoteelas ho $h_0 = \frac{v^2}{2g}$ v = velocity of liquid of pipe.5) Loss of head cleve to Bend in pipe! when there is bend in pipe , the nelocity of flow changes due to which formation of eddies Takes place. $\frac{h_b = \frac{1}{2g}}{h_b} = \frac{1}{2g} = \frac{$ hb = olom of head due to bend. K= wefficient of bend. 6) LOAN Of Head in Various pipe Littings. This is the low of head in various pipe fittings. 9+ in expressed as Kv2] V= whomby of flow.

K = coefficient of pipe till

HYDRAULIC GRADIENT LINE :-

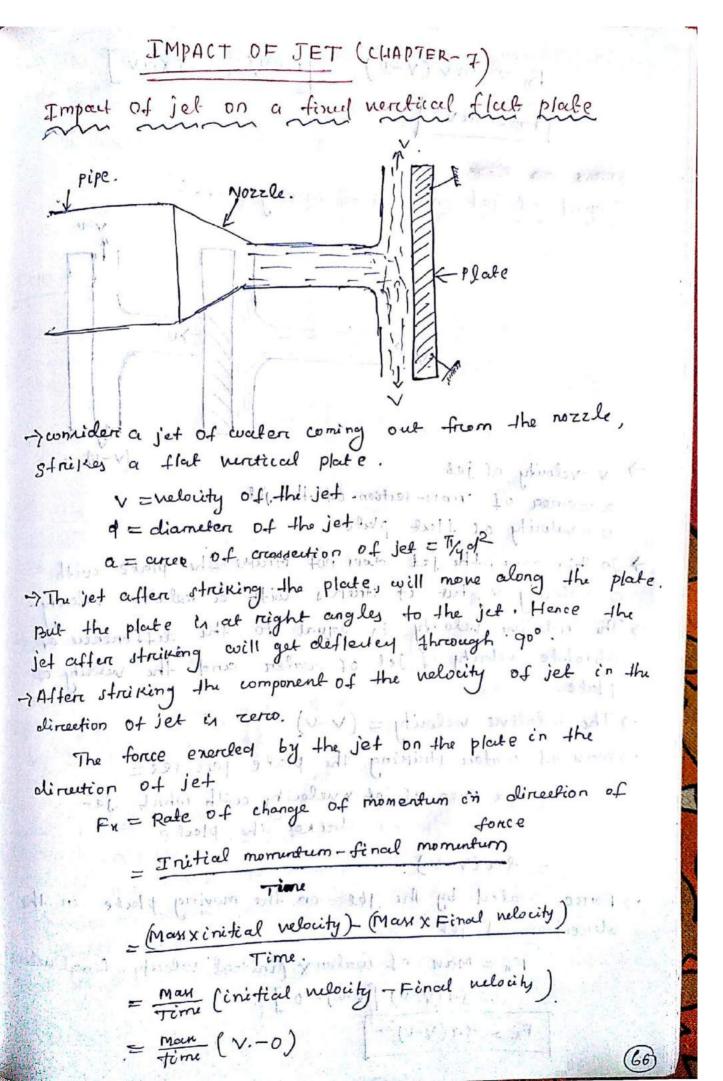
gt is defined as the line which gives the sum of pressure head (P/w) and datum head(Z) of a flowing fluid in a pipe with respect to some reference line.

Jet is briefly written as H.G.L (Hydraulic gradient)

TOTAL ENERGY LINE!

9+ in defined on the line which gives the rum of pressure head, datum head and rinetic head of a flowing fluid in a pipe with respect to some resterence line.

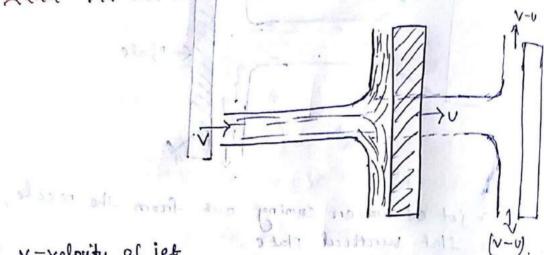
The briefly written on FE.L (Total Energy Line).



$$F_n = \frac{\beta \alpha V (V-0)}{F_{\mathcal{X}} = \frac{\beta \alpha V (V-0)}{F_{\mathcal{X}} = \frac{\beta \alpha V (V-0)}{F_{\mathcal{X}}}}$$

Former Cap Petrack

Impact of jet on ventical moving plate:



> v=velocity of jet a = curea of cross-section of the jet v = relocity of flat plate : Il la notione.

-> In this care, the jet does not streike the plate with a nelocity v, but it strickes with a relative velocity. > The relation velocity is equal to the difference of absolute relocity of jet of evaler and the relocity of

-> The relative velocity = (V-V)

-> Man of water striking the plate per see = fx Area of jet x velocity couth which jet strainer the plante = fer (V-U).

-> Force enerted by the jet on the moving place in the

Fn = Man of water X (initial velocity - final velow) = 8a(v-v) [(v-v)-0] Fx = 3a(v-v)2

-> The work will be done by the jet on the place au plate is moving. workdone = Force x relocity = FXX U $W = fa(V-U)^2 \chi U$ enerted by a jet of coaler, on a series of varies -> In actual practice, a large number of plates are mounted on the circumferoneu of a wheel at a fined distance -> The jet strikes a plate and due to the force energices by the jet on the place, the wheel stands moving. N= relocity of jet. d = diameter of jet. jet = 1/4 d 2

a = cross-sectional area of jet = 1/4 d 2 U = velocity of varie. -> man of water per second strucking the services of -) jet struckes the place with a relocity = (v-v)

-> The force enembed by the jet in the direction of motion of plate Fr = mous of x (initial relocity - final relocuty = 3 av[(v-v)-0] Fr = fav(v-v) workdone = Force & Distance velocity W = fav (v-v) x v printic energy of the jet per second = 1/2mv2 = 1/2 av x v2 KE = 1/2 9 av 3 1= workdone per recond $=\frac{\operatorname{fav}(v-u)\times u}{1/2\operatorname{fav3}}=\frac{\operatorname{zu}(v-u)}{\sqrt{2}}$ condition for Maximum Efficiency dn = 0 => d (20 (V-U)) = 0. $\Rightarrow \frac{d}{dv} \left(\frac{2vv - 2v^2}{v^2} \right) = 0$ $\Rightarrow \frac{2v - 2x 2v}{v^2} = 0$ =) 24-40=0 $=> V = 20. = \sqrt{0 = \frac{1}{2}}$

Manimum efficieny
$$\eta_{\text{man}} = \frac{2v(v-v)}{v^2}$$

$$= \frac{2v(2v-v)}{(2v)^2}$$

$$= \frac{2v \times v}{4v^2} = \frac{1}{2} = \frac{5v}{2}, \quad \square$$

$$\eta_{\text{max}} = \frac{5v}{2}.$$

on a moving curved plate of ine will plainter in pullin our He by it was in the direction ing interest and interesting -> As the st jet strickes tangentially, the loss of energy ofm to impact of the jet will be zero. as the plate is moving, the velocity with which jet of valer staines is equal to the relative velocity of the jet with respect to the plate. VI = velocity of the jet at inlet U1 = velocity of vare at inlet Vry = relative velocity of jet and plate at inlet. d=blade angle (inlet) 0 = vane angle (inlet) V2 = velocity of jet at outlet. U2 = velocity of vare at outlet. Vrz = relative vilouity of jet at outleet. 13 = black angle at outlet. φ ≈ voine cengle at outlet.



